

Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

- 1-20. Cancelled.
21. (Original) Macrostructures prepared by a process comprising the steps of
- (a) forming a composite material composed of a porous organic ion exchanger having a three-dimensional pore structure and a continuous matrix of a mesoporous inorganic material within the three-dimensional pore structure of the porous organic ion exchanger; and
 - (b) removing the porous organic ion exchanger from the composite material to yield the macrostructures
 - (c) treating said continuous three-dimensional matrix of mesoporous inorganic material, before or after removal of said porous organic ion exchanger from the composite material, under hydrothermal conditions to convert at least a portion of said mesoporous inorganic material to a crystalline molecular sieve composition.
22. (Original) The macrostructures of claim 21, wherein in the process the step of treating said continuous three-dimensional matrix of mesoporous inorganic material under hydrothermal conditions is conducted in the presence of a structuring agent to convert at least a portion of said porous inorganic material to a crystalline molecular sieve composition.
23. (Original) The macrostructures of claim 21, wherein in the process the step of treating under hydrothermal conditions occurs before the step of removing the porous organic ion exchanger from the composite material.

24. (Original) The macrostructures of claim 21, wherein in the process the step of treating under hydrothermal conditions occurs after the step of removing the porous organic ion exchanger from the composite material.
25. (Original) A process for converting hydrocarbons comprising contacting a hydrocarbon feedstream under hydrocarbon conversion conditions with a catalyst having macrostructures comprised of a crystalline molecular sieve composition prepared by a process comprising:
- (a) forming a composite material composed of a porous organic ion exchanger having a three-dimensional pore structure and a continuous matrix of a mesoporous inorganic material within the three-dimensional pore structure of the porous organic ion exchanger; and
 - (b) removing the porous organic ion exchanger from the composite material to yield the macrostructures
 - (c) treating said continuous three-dimensional matrix of mesoporous inorganic material, before or after removal of said porous organic ion exchanger from the composite material, under hydrothermal conditions to convert at least a portion of said mesoporous inorganic material to a crystalline molecular sieve composition.
26. (Original) The process recited in claim 25, wherein the step of treating said continuous three-dimensional matrix of mesoporous inorganic material under hydrothermal conditions is conducted in the presence of a structuring agent to convert at least a portion of said mesoporous inorganic material to a crystalline molecular sieve composition.
27. (Original) The process recited in claim 25, wherein the step of treating under hydrothermal conditions occurs before the step of removing the porous organic ion exchanger from the composite material.
28. (Original) The process recited in claim 25, wherein the step of treating under hydrothermal conditions occurs after the step of removing the porous ion organic exchanger from the composite material.

29. (Original) The process recited in claim 25, wherein said macrostructures have a size and shape of the three-dimensional pore structure of said porous organic ion exchanger.
30. (Original) The process recited in claim 29, wherein said porous organic ion exchanger is a porous organic anionic ion exchanger.
31. (Original) The process recited in claims 25, wherein the hydrocarbon conversion process is selected from the group consisting of cracking of hydrocarbons, isomerization of alkyl aromatics, transalkylation of aromatics, disproportionation of alkylaromatics, alkylation of aromatics, reforming of naphtha to aromatics, conversion of paraffins and/or olefins to aromatics, and conversion of oxygenates to hydrocarbon products.
32. (Original) The process recited in claim 25, wherein said hydrocarbon conversion is carried out at conditions comprising a temperature of from 100°C to 760°C, a pressure of 0.1 atmosphere to 100 atmospheres, a weight hourly space velocity of from 0.08 hr⁻¹ to 200 hr⁻¹.